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# A Techno-Economic Assessment of Hydrogen Production by Gasification of Biomass

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# **Project Team**

- > Project sponsored by U.S. Dept. of Energy (EERE), Hawaii Electric, Gas Technology Institute (GTI), Electric Power Research Institute (EPRI), and the University of Hawaii.
- > DOE Program Manager: Mr. Douglas Hooker

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# **Project Objectives**

- Determine the technical and economic potential of producing hydrogen from biomass with an end-use in PEM fuel cells
- > Project outline:
  - > Develop a biomass resource assessment
  - > Collect information on feeding systems
  - > Simulate gasification with biomass
  - > Determine gas cleaning requirements
  - > Determine hydrogen production costs
  - > Assess public programs and initiatives
  - > Determine barriers to commercialization



# **Project Timeline**

| Task |     | Task Name  | Months From Start of Project |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|------|-----|--|------------------------------|-----|-----|-----|-----|------|-------|-----|-----|-----|------|----|----|----|----|
|      |     |  | 01                           | 02  | 03  | 04  | 05  | 06   | 07    | 08  | 09  | 10  | 11   | 12 | 13 | 14 | 15 |
| 1.0  |     | Resource Assessment of Biomass Feedstocks                  |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      | 1.1 | Bagasse, Switch Grass, and Nut Shell Availability and Cost |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      | 1.2 | Process Scale Determination                                |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
| 2.0  |     | Hydrogen Production via Gasification/Pyrolysis of Biomass  |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      | 2.1 | Identification/Evaluation of Solids Handling Systems       |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      | 2.2 | Modeling for Gasification of Three Feedstocks and Analysis |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      | 2.3 | Gas Purification/Cleanup Requirements                      |                              |     |     | •   |     | 8    |       |     |     |     |      |    |    |    |    |
| 3.0  |     | Cost of Hydrogen Production and Cost Sensitivity Analysis  |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
| 4.0  |     | Assessment of Public Programs and New Policy Initiatives   |                              |     |     |     |     |      |       |     |     | •   | •    | (  |    |    |    |
| 5.0  |     | Market Barries and Commercial Opportunites                 |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
| 6.0  |     | Final Report   |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      |     |  |                              |     |     |     |     |      |       |     |     |     |      |    |    |    |    |
|      |     | Figure 2. Project Schedule (Start Date: September          | 15,                          | 200 | 1/1 | End | Dat | e: [ | De ce | emb | oer | 15, | 2002 | 2) |    |    |    |



# **Project Relevance**

- > Biomass represents an alternative, low cost fuel source that has potential to produce a high value end product, hydrogen.
- > Biomass gasification is a source of nonfossil based energy and chemical production.
- > Hydrogen production from domestic biomass resources can alleviate foreign dependence on fossil fuels while producing a clean fuel for PEM fuel cells.



# **Technical Approach**

- > A resource assessment was performed to determine plant size capacities
- > A GTI proprietary, empirical model was used to simulate gasification of biomass
- > A HYSYS® design and simulation package was used to simulate hydrogen production
- The economic analysis was performed utilizing data from EPRI's existing database



# **Project Assumptions**

#### **Technical Assumptions for Gas Purification**

- Fuel gas can be cleaned at gasifier temperature
- Reformer Requirements
  - > H<sub>2</sub>S less than 100 ppmv
- PEM Fuel Cell Requirements
  - > H<sub>2</sub>S less than 1 ppmv
  - > NH<sub>3</sub> less than 1 ppmv
- > CO less than 10 ppmv 80% recovery in PSA with 99.9% purity H<sub>2</sub>

### **Economic Assumptions**

- Power law scaling for increased capacity
- Linear hydrogen production with increased plant size capacity

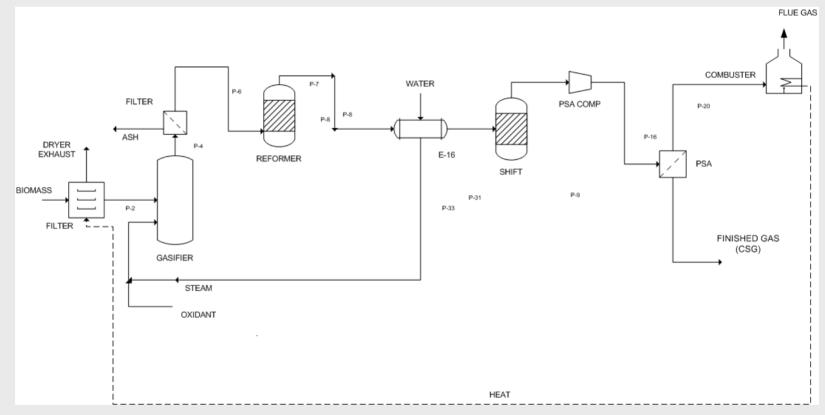


#### **Resource Assessment**

- > Three Feedstocks Selected:
  - Bagasse, Switchgrass, and a Nutshell Mix
- > Bagasse
  - Delivered cost of \$30 40 / tonne
  - Potential availability of 700 5200 tonnes / day
- > Switchgrass
  - Delivered cost of \$27 46 / tonne
  - Availability undetermined
- > Nutshell Mix
  - 40% almond shell, 40% prunings, 20% walnut shells
  - Delivered cost of \$12 44 / tonne
  - Potential availability of 500 tonnes / day



# **Process Flow Diagram**





**Bagasse Process Flow Diagram** 

## **Simulation Results**

|  | Bagasse | Switchgrass | Nutshell Mix |
|--|---------|-------------|--------------|
| Heat Used in Reformer [GJ/h]                         | 24.8    | 25.7        | 24.2         |
| Heat Used in Dryer [GJ/h]                            | 45.8    | 0           | 0            |
| Heat Recovered from PSA Reject [GJ/h]                | 60.0    | 80.5        | 89.0         |
| Heat Recovered from Reformer Stream [GJ/h]           | 19.1    | 8.1         | 5.3          |
| Net Heat from the system [GJ/h]                      | 8.5     | 62.9        | 70.1         |
| Power Used in PSA Compressor [GJ/h]                  | 6.97    | 8.20        | 8.45         |
| Power Used for Air Separation [GJ/h]                 | 5.90    | 5.10        | 4.10         |
| Total Heating Value of H <sub>2</sub> Product [GJ/h] | 186     | 220         | 230          |
| Total Heating Value of Dry Biomass Feed [GJ/h]       | 297     | 342         | 361          |
| Cold Efficiency                                      | 0.628   | 0.644       | 0.637        |
| Effective Thermal Efficiency                         | 0.583   | 0.744       | 0.756        |
| H <sub>2</sub> / Dry Biomass [g/kg]                  | 78.1    | 84.1        | 88.3         |



BASIS: 500 tonnes / day at gasifier fed moisture content

## **Economic Results**

|              | Gasifier<br>Feed Rate | Hydrogei | n Produced | Feedstock<br>Cost | Capital<br>Cost  | H <sub>2</sub> Cost<br>15% IRR |
|--------------|-----------------------|----------|------------|-------------------|------------------|--------------------------------|
| Feedstock    | Dry Tonnes /<br>Day   | Tonnes / | Nm³ / Day  | US \$ / GJ        | US \$<br>Million | US \$ / GJ                     |
|              | 400                   | 31.2     | 347,000    | 1.50              | 37.0             | 9.13                           |
| Bagasse      | 800                   | 62.5     | 695,000    | 1.50              | 61.1             | 7.64                           |
|              | 1600                  | 125      | 1,390,000  | 1.50              | 100.9            | 6.57                           |
|              | 440                   | 37.0     | 412,000    | 1.50              | 36.5             | 7.95                           |
| Switchgrass  | 880                   | 74.0     | 824,000    | 1.50              | 60.6             | 6.73                           |
|              | 1760                  | 148      | 1,648,000  | 1.50              | 100.9            | 5.86                           |
| Nutshell Mix | 438                   | 38.7     | 488,000    | 1.50              | 36.3             | 7.72                           |



#### **Commercialization Barriers**

- > Technical Barriers
  - Materials handling
  - Cleaning and purification
- > Economic Barriers
  - Hydrogen infrastructure (chicken and egg)
  - Supply and demand of waste crops
  - High cost fuel compared to available sources
- > Psychological Barriers
  - Hindenburg and Challenger disasters
  - Educational programs



#### **Conclusions**

- > Hydrogen Can Be Produced Economically From Biomass
  - Costs are competitive with SMR and potentially better with lowered fuel costs through the inception of public programs
- > Areas Deserving Further Research
  - Gas Clean Up
  - Membrane Separation
  - Feeding Systems
  - Development of a Hydrogen Infrastructure



#### **Future Plans**

- > Address the technical issues found in the conclusion of this report
- > Build on the expertise gained in this paper study and apply it to an experimental study of hydrogen production from biomass
- Commercialize the process of hydrogen production from biomass gasification using GTI's fluidized bed, RENUGAS technology



# **2002 Merit Review Responses**

#### > Comment:

 Would it make more sense to take a low-tech approach to crop residue? If burning it to make steam and generate electricity is not profitable, then trying to make hydrogen will not be either.

#### > Response:

 Electricity production is more efficient using gasification than combustion. Energy is also not the only use for hydrogen. Hydrogen produced from biomass for other processes may prove more cost effective.

